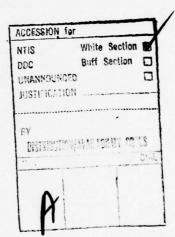
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surface roughness body data were obtained at zero and three degrees angle of attack. High speed cine Schlieren Photographs of the model bow shock structure and dynamics were obtained.



Hypersonic Heat Transfer Test Program in the VKI Longshot Facility

Test Summary Report

V. DiCristina

19 January 1979

AVSD-0028-79-CR

Contract No. F49620-78-C-0029

Prepared For

Department of the Air Force Air Force Office of Scientific Research (AFSC) Bolling Air Force Base, D.C. 20332

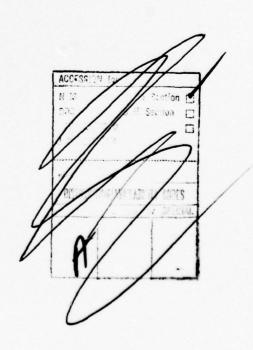
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# CONTENTS

		PAGE
1.0	INTRODUCTION AND SUMMARY	1
2.0	DISCUSSION	. 2
	2.1 TEST FACILITY	. 2
	2.2 MODEL DESIGN	. 2
	2.3 INSTRUMENTATION	. 2
	2.4 TEST MATRIX	. 3
	2.5 TEST RESULTS	4



## 1.0 INTRODUCTION AND SUMMARY

A series of tests were performed in the Longshot Facility of the Von Karman Institute for Fluid Dynamics (VKI) in Rhode-St. Genese, Belgium in support of USAF Great AFOSR 78-3474 This post test report is a summary of sixteen tests conducted in the Longshot Facility during the periods of 5-16 June 1978 (Phase I) and 18-29 September 1978 (Phase II). The complete test results are included in the VKI post test report.

The purpose of these tests was to measure local pressure and heat transfer distributions on a concave body configuration over a range of Mach number and Reynold number conditions. Both small and large surface roughness body data were obtained at zero and three degrees angle of attack.

The calorimeter instrumentation was calibrated at VKI during the period 24-28 April 1978. The instrumented test model was delivered to the VKI facility for the first series of tests on 5 June 1978. All data measurements were made as planned including high speed cine schlieren photographs of the model bow shock structure and dynamics.

The results of the first eight tests are included here, the complete data set including the large roughness body data will be issued as part of the final VKI test report.

## 2.0 DISCUSSION

## 2.1 TEST FACILITY

The VKI Longshot facility was used for this program. Longshot differs from a conventional gun tunnel in that a heavy piston is used to compress the nitrogen test gas to very high pressure and temperatures. The test gas is then trapped in a reservoir at peak conditions by the closing of a system of check values. The flow conditions decay monotonically during 20 milliseconds running time as the nitrogen trapped in the reservoir flows through the  $6^{\circ}$  half angle conical nozzle into the pre-evacuated open jet test chamber. The maximum supply conditions used in these tests are approximately  $60,000 \text{ lb/in}^2$  at  $1900^{\circ}\text{K}$  to  $2350^{\circ}\text{K}$ . These conditions provide unit Reynolds numbers of  $8.5 \times 10^{\circ}$  per foot at a Mach number of 16 and  $3.5 \times 10^{\circ}$  at M = 20.

## 2.2 MODEL DESIGN

The test model design was a concave body configuration shown in Figure 1. This model configuration was designated as model M. The model was fabricated from 303 stainless steel having a wall thickness of approximately 0.2 inches. The first series of tests (runs 1-8) were performed with a small 5 mil roughness over the model surface. The rough surface was achieved by sand blasting. The second series of tests (runs 9-16) were performed with large 65 mil roughness elements over the model surface. The large roughness was created by bonding aluminum spheroid particles onto a sprayed adhesive and coated with a sprayed acrylic. The local calorimeter and pressure port areas did not contain roughness elements.

## 2.3 INSTRUMENTATION

The test model was instrumental with both pressure and heat flux gages. The gage locations are shown in Figure 1. The test model contains eleven heat flux gages and nine pressure taps. Only eight pressure measurement channels were available at the test facility. The last pressure tape on the concave surface was not connected. PCB model 112A21 high resolution pressure tranduces were connected through short flexible tubes to the surface taps.

The heat transfer gages are smooth calorimeter discs fabricated from .004 inch high conductivity copper stock. A l mil wire chromel alumel thermocouple is welded to the copper disc which is bonded to an insulating holder. Twenty calorimeters were fabricated and calibrated at the VKI facility. Table I lists the measured calibration constant ( $C_T$ ) for each gage. The values shown are the coverage of two measurements. The actual measured disc thickness ( $X_A$ ) is also shown compared with the calculated effective disc thickness (XE). The data was derived from the following relationships:

$$c_{T} = \frac{\dot{Q}_{C}}{\Delta E/\Delta t}$$

$$x_{E} = \frac{c_{T}}{\rho c_{P}} = .00523 c_{T}$$

where:  $\dot{Q}_{C}$  = calibration heat flux  $\Delta E/\Delta t$  = thermocouple EMF output  $X_{E}$  = Effective gage thickness  $C_{T}$  = Calibration constant  $\rho$  = Density, copper  $C_{p}$  = Specific heat, copper

The variations in  $\mathbf{X}_{\mathrm{E}}$  are due to the thermocouple weld joints.

### 2.4 TEST MATRIX

The matrix for the sixteen runs made in the Phase I and II test series is shown in Table II. The small surface roughness model is designated as MRl and the large roughness model as MR2. The pressure and heat transfer gages were intermixed on the model surface as shown in Figure 1. In order to obtain a complete distribution of pressure and heat transfer measurements for the angle of attack cases both a positive and negative incidence angle was run for the same test conditions as shown in Table II.

### 2.5 TEST RESULTS

The data measurements for each run included surface pressure, heat transfer and schlieren photos of the model flow field.

The model flow field and bow shock structure was recorded using a 6000 spark per second cine schlieren system. Figures 2 and 3 show the recorded bow shock time sequence. As expected the model contour generates an unstable flow field which results in an oscillating bow shock. The observed oscillations indicate a frequency of 1500-2000 cps. The Strouhal number which depends on the flow frequency (f), model diameter (d), and freestream velocity ( $V_{\omega}$ ) is:

 $St = Df/V_{ap}$ 

From the observed oscillations the average Strouhal number appears to be St = 0.13 which is about 30% lower than previously observed from tests at M $_{\infty}$  = 10 and Re $_{\infty}$  = 8 x 10 $^6$  ft<sup>-1</sup>.

The measured pressure distributions are shown in Figures 4 to 11. The pressure data has been normalized with respect to the measured pitot pressure measurement. The heat transfer distributions are shown in Figures 12 to 19. The heat transfer data are the measured values for each run condition.

TABLE I

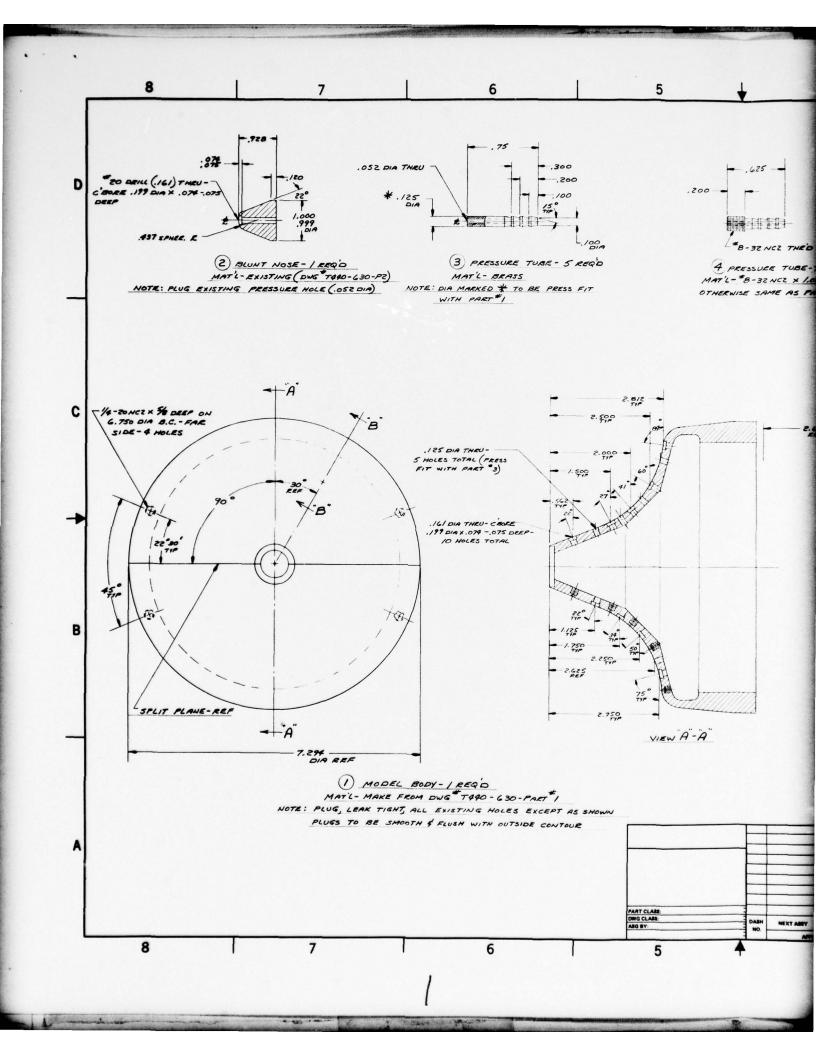
Heat Transfer Gage Calibration Data

Gage No.	Avg. Calib. Coeff., C <sub>T</sub>	Effect. Gage Thickness, X <sub>E</sub> (in.)	Actual Gage Thickness (in.)
1	.733	.0038	.0031
2	.671	.0035	.0036
3	.530	.0028	.0035
4	.555	.0029	.0038
5	.654	.0034	.0038
6	.548	.0029	.0032
7	.480	.0025	.0034
8	.456	.0024	.0036
9	.495	.0026	.0034
10	.667	.0035	.0038
11	.783	.0041	.0037
12	.951	.0050	.0035
13	.580	.0030	.0031
14	.606	.0032	.0034
15	.612	.0032	.0034
16	.626	.0033	.0037
17	.595	.0031	.0036
18	.585	.0031	.0035
19	.505	.0026	.0036
20	.676	.0035	.0033

TABLE II

VKI Longshot Test Matrix

Run No.	Model	(degree)	M <sub>OO</sub>	$R_{e_{QQ}}(ft^{-1})$
		Phase I		
1	MR1	0	20	$2.0 \times 10^6$
2	MRl	0	20	$3.3 \times 10^6$
3	MRl	0	16	$4.5 \times 10^6$
4	MR1	0	16	$8.6 \times 10^6$
5	MR1	+3	20	$3.3 \times 10^6$
6	MRl	-3	20	$3.3 \times 10^6$
7	MRl	+3	16	$6.6 \times 10^6$
8	MR1	-3	16	$8.6 \times 10^6$
		Phase II		
9	MR2	0	20	$2.0 \times 10^6$
10	MR2	0	20	$3.3 \times 10^6$
11	MR2	0	16	$4.5 \times 10^6$
12	MR2	0	16	$8.6 \times 10^6$
13	MR2	+3	20	$3.3 \times 10^6$
14	MR2	-3	20	$3.3 \times 10^6$
15	MR2	+3	16	$8.6 \times 10^6$
16	MR2	-3	16	$8.6 \times 10^6$



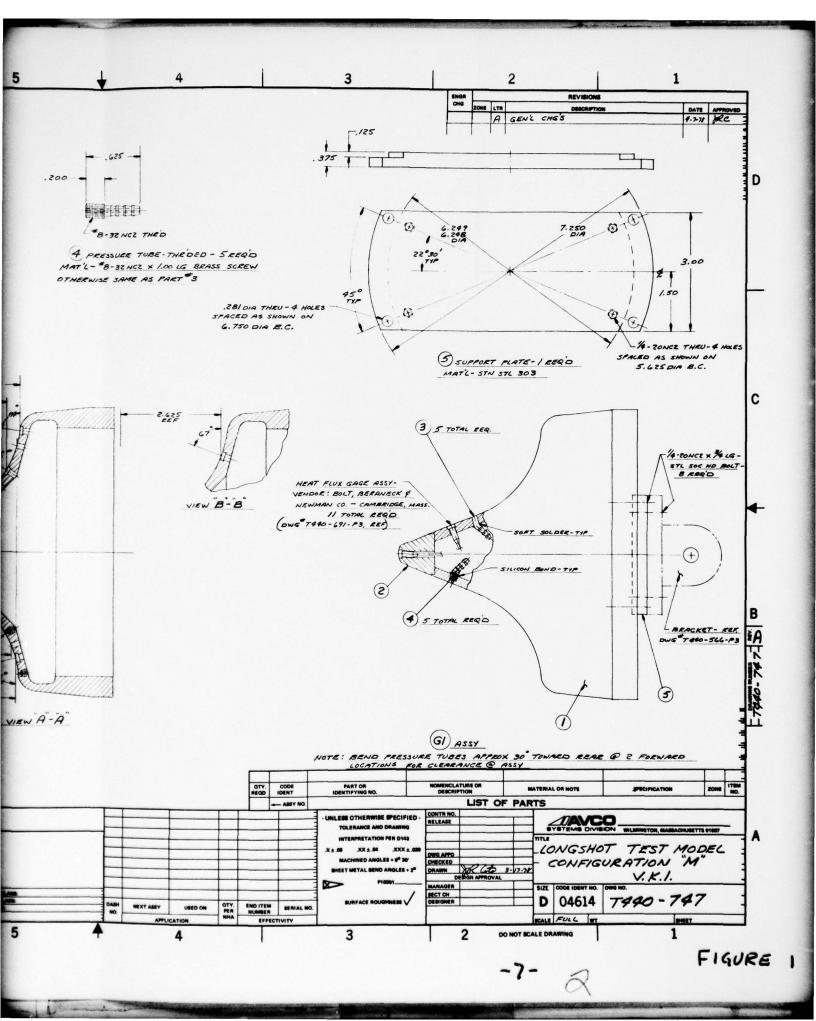
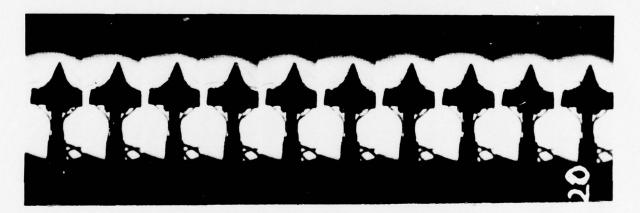


FIGURE 2a
Cine Schlieren Flow Field
Run No. 593 Model MR1  $M_{\infty} = 16$ ,  $R_{e_{\infty}} = 8.6 \times 10^6/\text{ft}$ ,  $\alpha = -3^\circ$ 



Frame 1



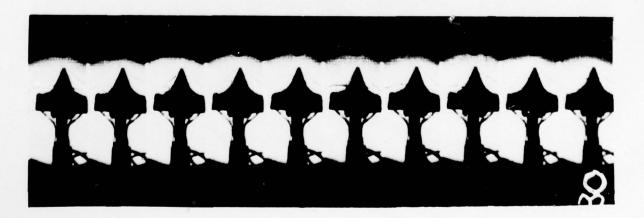
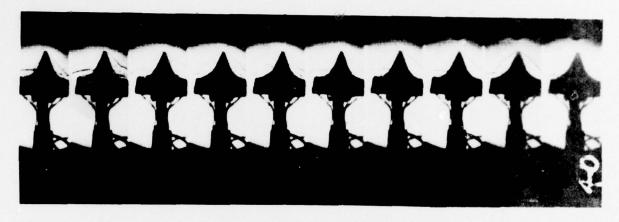
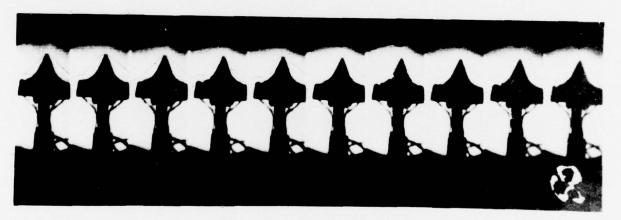


Figure 2b Ciné Schlieren Flow Field Run No. 593 Model MR1 Model 16, Re $_{\infty}$  = 8.6 x 10 $^{6}/\text{ft}$ ,  $\alpha$  = -3 $^{\circ}$ 



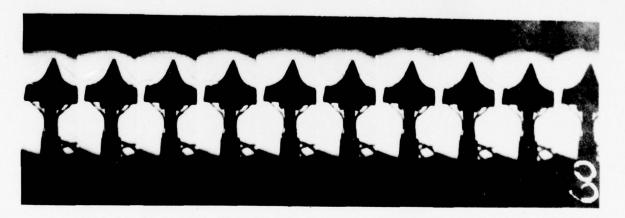
Frame 31

40



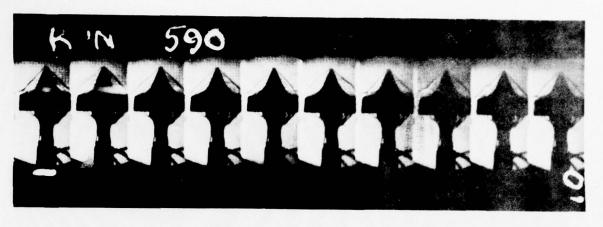
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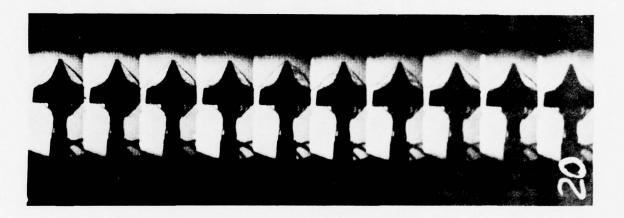


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Figure 3a
Cine Schlieren Flow Field
Run No. 590 Model MR1  $M_{\infty} = 20$ ,  $R_{e_{\infty}} = 2.0 \times 10^6/\text{ft}$ ,  $\alpha = 10^6$ 



Frame



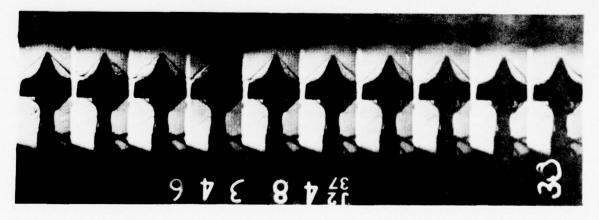
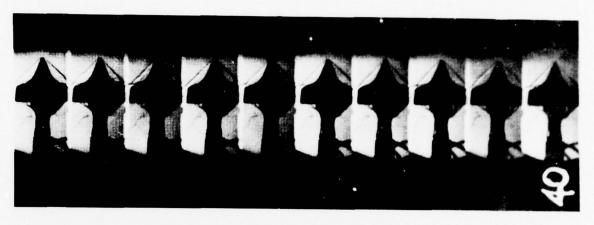
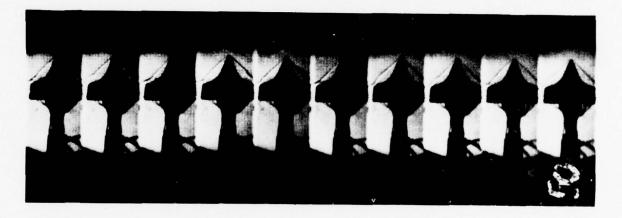


Figure 3b
Cine Schlieren Flow Field
Run No. 590 Model MR1
M = 20, R<sub>e</sub> = 2.0 x 10<sup>6</sup>/ft, **x** = 0



Frame 31



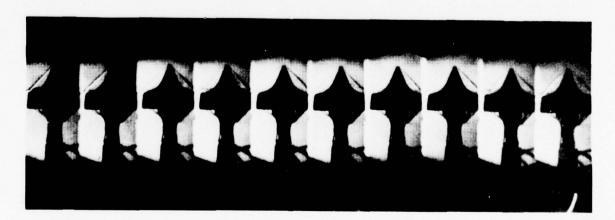


FIGURE NO. 4
WALL PRESSURE ON CONCAVE BICONIC

٠										9	
MRI	590		$R_{e_{m}} = 2.0 \times 10^{6} \text{ Fr}^{-1}$							2	
MODEL	RUN NO.	$M_{\infty} = 20$	Re = 2.0	$\alpha = o^c$				Q	)	4	HES
									0	3	DISTANCE ALONG BODY - INCHES
									0 0	2	ICE ALONG
									0		DISTA
				N 1.5	b <sup>^</sup> \b	,OIT	₽¥	якеззике	O MALL I		90

FIGURE NO.  $\mathcal S$  WALL PRESSURE ON CONCAVE BICONIC

	MRi	589		Re = 3.3 × 10 <sup>6</sup> Fr <sup>-1</sup>						10
0.000	MODEL	RIIN NO.	$M_{\infty} = 20$	Re = 3.3	$\alpha = 0^{\circ}$				0	4 HES
STREET TARGET ON CONCENT FIRM									0	3 4 BODY - INCHES
NO THEODOR								C	0	2 DISTANCE ALONG
1									0	1 DISTA
										C
					N 1.5	P <sub>w</sub> /P	OIT.	ъ ая∪геая г°	WALL D	

MAVCO

FIGURE NO. 6
WALL PRESSURE ON CONCAVE BICONIC

									T	
									,c	
MRI	588	$M_{\infty} = /6$ $R_{\infty} = 4.5 \times 10^6 \text{ FT}^{-1}$							2	
 MODEL	RUN NO.	$M_{\infty} = 1/6$ $R_{\infty} = 4.5$	$\alpha = 0^{\circ}$			0			4	нез
							0		3	DISTANCE ALONG BODY - INCHES
						o	0		2	JCE ALONG
							0			DISTA
			N 1.5	a/ <sup>M</sup> a	OIT.	SSURE R	ъве	MALL		

MAVCO

FIGURE NO. 7
WALL PRESSURE ON CONCAVE BICONIC

										.0	
MRI	586		x 10 <sup>6</sup> FT <sup>-1</sup>							2 ا	
MODEL	RUN NO.	91 = 0 W	$R_{e} = 8.6 \times 10^6 \text{ Fr}^{-1}$	$\alpha = 0^{\circ}$					0	4	HES
									0	3	DISTANCE ALONG BODY - INCHES
									o o		CE ALONG
									0	7	DISTAN
				N 1.5	d/ <sup>M</sup> d	, OIT	M	я го го	MALL E		

MAVCO

FIGURE NO. **8**WALL PRESSURE ON CONCAVE BICONIC

					(a)								
	MRI	261/265		106 FT <sup>-1</sup>	Q = +3 (WINDWARD)							.0	
271122	MODEL	RUN NO.	$M_{\infty} = 20$	Re = 3.3 k 106 FT-1	$\alpha = +3$				0			4	HES
WALL FRESSORE ON CONCAVE BICONIC										0		3	BODY - INC
NESSONE ON										0		2	DISTANCE ALONG BODY - INCHES
Manna F										0			DISTA
					N 1.5	<sup>†</sup> d∕ <sup>™</sup> d	OIT.	M	RESSURE.	MALL E	0		

MAVCO

FIGURE NO. **Q**WALL PRESSURE ON CONCAVE BICONIC

MRI	541/545		Re = 3.5 × 10 <sup>6</sup> FT <sup>-1</sup>	$\alpha = -3^{\circ}$ (LEEWARD)							2	
MODEL	RUN NO.	$M_{\infty} = 20$	Re_ = 3.5	$\alpha = -3^{\circ}$					0		4	неѕ
									0		3	DISTANCE ALONG BODY - INCHES
								0	0		7	NCE ALONG
									0		1	DISTA
											C	
				N 1.5	₽ <sub>w</sub> √₽	OIT.	м	жезѕике .	MALL E	0		

ZAVCO

FIGURE NO. 10
WALL PRESSURE ON CONCAVE BICONIC

					ARD)						,c	
	MRI	593/594		k 10 <sup>6</sup> FT <sup>-</sup>	(X = + 5 (WINDWARD)						2	
TCONTC	MODEL	RUN NO.	91 = 0 W	Re_ = 8.6 k 10 <sup>6</sup> FT <sup>-1</sup>	$\alpha = +5$				0		4	HES
WALL PRESSURE ON CONCAVE BICONIC										0		DISTANCE ALONG BODY - INCHES
ESSURE ON										0		CE ALONG
WALL FR										0	2	DISTAN
					N 1.5	d/ <sup>M</sup> d	,OIT	A.R.	экезгике	MALL E		

FIGURE NO. 11
WALL PRESSURE ON CONCAVE BICONIC

				(0)							.0	
MR1 502 (501	+1C/CtC		$R_{e_{m}} = \theta.6 \times 10^{6} \text{ Fr}^{-1}$	$\alpha = -3$ ° (LEEWARD)							2	
	KUN NO.	9/ = 8 <sub>M</sub>	$R_{e} = \theta.6$	$\alpha = -3$					0		t	HES
									0		3	DISTANCE ALONG BODY - INCHES
									0 0			ICE ALONG
									0		-2	DISTAN
											T	
				N 1.5	d/™d	OIT.	₽¥	eressure.	MALL I	0	Q_	

FIGURE NO. 12

									9	
E BICONIC							0	0	4	- INCHES
CONCAVI								0	<u>~</u>	
HEAT TRANSFER ON CONCAVE BICONIC	MRI	240		Re= 2.0 x 10 <sup>6</sup> FT <sup>-1</sup>				0 0	2	DISTANCE ALONG BODY
HEAT TR	MODEL	RUN NO. 540	M = 20	Re= 2.0				0	1	DIST
							0		0	
					300	STU/FT.	яз <b>т</b> гият	<b>НЕАТ</b> ○		

FIGURE NO. 13

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ONIC							0	o		неѕ
HEAT TRANSFER ON CONCAVE BICONIC								0	3	BODY - INCHES
NOFFER ON C	MRI	589		Re=3.3 × 106 FT	•			0 0	2	DISTANCE ALONG BODY -
HEAT TR	MODEL	RUN NO. 589	$M_{\infty} = 20$	Re= 3.3	a = 0°			0	1	DIST
									0	
					300 EC	2 TTT\UTE	телатек С			

MAVCO

FIGURE NO. 14

									9	
									5	
CONIC				0		0	0 0		4	INCHES
CONCAVE BI							0	0	3	
HEAT TRANSFER ON CONCAVE BICONIC	MRI	588		Rea=4.5 x 106 FT-1				0 0	2	DISTANCE ALONG BODY -
HEAT TR	MODEL	RUN NO.	$M_{\infty} = 16$	Re = 4.5	a = 0°			0	1	DIST
								>1 1/1	0	
					300	2 TTA\UTA	- <b>яззекат</b> 100	теан		
	<u> </u>									

0 HEAT TRANSFER ON CONCAVE BICONIC 0 DISTANCE ALONG BODY - INCHES 0 FIGURE NO. 15 0  $R_{e_{\infty}} = \theta, \epsilon_{\infty} = 10^6 \text{ Fr}^{-1}$   $\alpha = 0$ 0 RUN NO. 586 MR 0 M = 16 MODEL 0 300 100 BTU/FT HEAT TRANSFER

JAVCO

FIGURE NO. 16

HEAT TRANSFER ON CONCAVE BICONIC

										ی	
										2	
						0					
ONIC							0	0			HES
BIC								0		4	INC
IVE							0				- 7
COINC					ARD)				0	3	BOD
NO NO		592		6 FT <sup>-1</sup>	VINDW				0		DISTANCE ALONG BODY - INCHES
INSE	Z	1115		× 10	3°(v				0	2_	ANCE
HEST INMISTER ON CONCAVE BICONIC	MODEL	RUN NO. 591/592	$M_{\infty} = 20$	Rea = 3.3 × 106 FT	a = + 3° (WINDWARD)				0		DIST
										1	
					0	0		0	C	0	
					300			100			
					EC	BTU/FT2	FER -	ENAST	TAƏH		

FIGURE NO. 17

									9	
									5	
CONIC							0	0	4	INCHES
CONCAVE BI					(02			0	3	BODY - IN
HEAT TRANSFER ON CONCAVE BICONIC	MRI	24:1545		Re=3.3 x 106 FT	3°(LEEWARD)			0 0	2	DISTANCE ALONG BODY -
HEAT TRA	MODEL	RUN NO. 591/592	$M_{\infty} = 20$	Rea= 3.3	a =-			0	7	DIST
									0	
					300 EC	S TTA\UTA	ткаи <b>з</b> тек -	HEAT	9	

FIGURE NO. 18
HEAT TRANSFER ON CONCAVE BICONIC

1											
									,	9	
	5									2	
ONIC				,			0				INCHES
BIC										4	,
AVE						3	0				- УС
CONC						VAR		0		m	BOI
NO			46		FT	IND	0				LONG
HEAT INNSFER ON CONCAVE BICONIC		MRI	RUN NO. 593/594		Re 28.6 × 106 FT	a = + 3° (WINDWARD)		0		7	DISTANCE ALONG BODY ~
TR			NO.	9/	8.6	+					IST
near		MODEL	RUN	9/= W	118	×			0		
				_		_					
	-				-				0	0	
						300	200	100			
						э	BTU/FT2	TRANSFER	TAEH		
	_							l		L	

MAVCO

FIGURE NO. 19

									9	
									5	
						C	0			
ONIC							0			неѕ
VE BIC								0	4	DISTANCE ALONG BODY - INCHES
ONC					(02			0	3	ВОД
ON C		4		FT-1	WA			0		ONG
FER	_	3/5/		106	337)			0		E AL
ANS	MRI	59		×	30			0	2	ANC
HEAT TRANSFER ON CONCAVE BICONIC	MODEL	RUN NO. 593/594	9/ = W	Re=8.6 × 10 <sup>6</sup> Fr <sup>-1</sup>	a = - 30 (LEEWARD)			0	1	DIST
									C	
					300	0	100	0		
						BTU/FT <sup>2</sup>	далент Т	ТАЭН		